PRONOUNCED EFFECT OF SULFATE ION ON CATALYTIC ACTIVITY OF ${\tt ZrO}_2-{\tt SnO}_2$ FOR ISOMERIZATION OF CYCLOPROPANE

Gong-Wei WANG, Hideshi HATTORI, and Kozo TANABE*

Department of Chemistry, Faculty of Science,

Hokkaido University, Sapporo 060

The catalytic activity of ${\rm ZrO}_2{\rm -SnO}_2$ containing 3 wt% of sulfate ion for the isomerization of cyclopropane has been found to be pronouncedly higher than that of a pure ${\rm ZrO}_2{\rm -SnO}_2$ and even higher than those of ${\rm ZrO}_2$ and ${\rm SnO}_2$ which contain 3 wt% of sulfate ion.

The enhancement of catalytic activities for acid-catalyzed reactions on the addition of SO_4^{2-} has been reported for certain metal oxides such as TiO_2^{-1} , TiO_2^{-1} , and TiO_2^{-1} , TiO_2^{-1} , and TiO_2^{-1} , and TiO_2^{-1} , were estimated to be TiO_2^{-1} , TiO_2^{-1} , TiO_2^{-1} , and TiO_2^{-1} , according to the indicator method. Thus, the former two are called solid super acids. In the present work, the effect of TiO_2^{-1} on the catalytic activity of TiO_2^{-1} for the isomerization of cyclopropane which is known to be catalyzed by acids was studied.

Zirconium oxide, SnO_2 , and ZrO_2 - SnO_2 were prepared from aqueous solutions of ZrOCl_2 , SnCl_4 , and $\mathrm{ZrOCl}_2+\mathrm{SnCl}_4$, respectively, by precipitation with ammonia water, followed by washing with deionized water and drying at $100\,^{\circ}\mathrm{C}$ for 24 h and then calcining at $500\,^{\circ}\mathrm{C}$ for 2.5 h. The oxides including SO_4^{2-} were prepared by immersing the hydroxides in solutions of $\mathrm{(NH}_4)_2\mathrm{SO}_4$ and evaporating them to dryness, followed by drying at $110\,^{\circ}\mathrm{C}$ for 24 h and calcining at $500\,^{\circ}\mathrm{C}$ for 2.5 h. The content of SO_4^{2-} was 2.9 wt%. The surface areas were measured by the B.E.T. method.

The isomerization of cyclopropane was carried out at 100 or 300°C by using a closed recirculation apparatus of 789 ml capacity. About 10 Torr cyclopropane was introduced over 0.4 g of catalyst evacuated at 500°C for 2 h. The reaction product was analyzed by gas chromatography.

The catalytic activities of ${\rm ZrO}_2$, ${\rm ZrO}_2{\rm -SnO}_2$ of different compositions, and ${\rm SnO}_2$ with and without the addition of 2.9 wt% ${\rm SO}_4^{-}$ are shown in Table 1, where the surface areas of the catalysts are also given. The activities per unit surface area of ${\rm ZrO}_2{\rm -SnO}_2$ (9:1), (7:3), (1:1), (3:7) and (1:9) with ${\rm SO}_4^{2-}$ at $100\,^{\circ}{\rm C}$ of reaction temperature were 7, 140, 9, 6, and 22 times higher than those of the catalysts without ${\rm SO}_4^{2-}$ at $300\,^{\circ}{\rm C}$ of reaction temperature, respectively. The activity of ${\rm ZrO}_2{\rm -SnO}_2$ (7:3) containing ${\rm SO}_4^{2-}$ was about 3 and 2 times higher than those of ${\rm ZrO}_2{\rm +SO}_4^{2-}$ which was reported previously. The isomerization reaction did not take place at 100°C over the catalysts without ${\rm SO}_4^{2-}$, while the reaction rate was too

Table 1.	The effect of SO_4^{2-}	on catalytic activity	of ZrO ₂ -SnO ₂ for
	isomerization of c		

Catalyst	Surface area m ² g-1	Reaction temp.	Activity ^{a)}	
(atomic ratio)			10 ⁻⁵ m	ol min $^{-1}$ g $^{-1}$
ZrO ₂	47.8	300	0.098	(0.21)
$zro_2^2 + so_4^{2}$	113	100	2.48	(2.19)
ZrO ₂ -SnO ₂ (9:1)	80.3	300	0.65	(0.81)
$2rO_2 - SnO_2(9:1) + SO_4^{2-}$	102	100	5.80	(5.69)
$ZrO_2^-SnO_2^-(7:3)$	72.6	300	0.034	(0.05)
$ZrO_2 - SnO_2 (7:3) + SO_4^{2-}$	129	100	9.06	(7.02)
ZrO ₂ -SnO ₂ (1:1)	52.2	300	0.34	(0.65)
$Zro_2^- Sno_2^- (1:1) + So_4^{2-}$	111	100	6.66	(6.00)
$ZrO_2 - SnO_2(3:7)$	59.8	300	0.70	(1.17)
$ZrO_2^-SnO_2^-(3:7) + SO_4^{2-}$	109	100	7.29	(6.69)
ZrO ₂ -SnO ₂ (1:9)	57.6	300	0.10	(0.17)
$2rO_2 - SnO_2(1:9) + SO_4^{2}$	110	100	4.14	(3.76)
SnO ₂	31.6	300	0.034	(0.11)
$\operatorname{SnO}_{2}^{2} + \operatorname{SO}_{4}^{2}$	84.3	100	4.25	(5.04)

a) The figures in parentheses are the activity per unit surface area $(10^{-7} \text{ mol min}^{-1}\text{m}^{-2})$.

high to measure at 300°C over the catalysts with SO_4^{2-} . It is noted that the acid strength of $\mathrm{ZrO}_2-\mathrm{SnO}_2+\mathrm{SO}_4^{2-}$ could not be measured by the indicator method, because the basic indicators which are used for the measurement of super acidity gave the colors different from those of the conjugated acids on the catalyst surface.

In conclusion, it should be emphasized that $2\text{rO}_2-5\text{nO}_2+5\text{O}_4^{2-}$ is expected to act as an efficient catalyst for various acid-catalyzed reactions.

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